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# Metagenomic-based analysis of biofilm communities for electrohydrogenesis: From wastewater to hydrogen



Cristiano Varrone<sup>a,1</sup>, Joy D. Van Nostrand<sup>b,1</sup>, Wenzong Liu<sup>c,\*\*</sup>, Benjamin Zhou<sup>b</sup>, Zhongshi Wang<sup>b</sup>, Fenghai Liu<sup>a</sup>, Zhili He<sup>b</sup>, Liyou Wu<sup>b</sup>, Jizhong Zhou<sup>b</sup>, Aijie Wang<sup>a,c,\*</sup>

<sup>a</sup> State Key Laboratory of Urban Water Resource and Environment, Harbin Institute of Technology (SKLUWRE, HIT), Harbin, China

<sup>b</sup> Institute for Environmental Genomics and Microbiology and Plant Biology, University of Oklahoma, United States <sup>c</sup> Research Center for Eco-Environmental Sciences, Chinese Academy of Sciences, Beijing, China

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#### ABSTRACT

Microbial electrolysis cells (MECs) use exoelectrogenic microorganisms to convert organic matter into H<sub>2</sub>, although yields can vary significantly with environmental conditions, likely due to variations in microbial communities. This study was undertaken to better understand how microbial communities affect reactor function. Using wastewater as inoculum, 15 MEC reactors were operated for >50 days and subsequently five reactors were selected for further analysis. Solution (26 mL) was collected every 3-4 days for DNA extraction. DNA was hybridized to GeoChip, a comprehensive functional gene array, to examine differences in the reactor microbial communities. A large variety of microbial functional genes were observed in all reactors. Performances ranged from poor (0.1  $\pm$  0.1 mL) to high (12.2  $\pm$  1.0 mL) H<sub>2</sub> production, with a maximum yield of 5.01  $\pm$  0.43 mol H<sub>2</sub>/mol<sub>elucose</sub>. The best performance was associated with higher cytochrome c genes, considerably higher exoelectrogenic bacteria (such as Shewanella, Geobacter), less methanogens and less hydrogen-utilizing bacteria. The results confirmed the possibility to obtain an effective community for hydrogen production using wastewater as inoculum. Not like fermentation, hydrogen production was significantly controlled by electron transporting process in MECs. GeoChip findings suggested that biofilm formation can be highly stochastic and that presence of dissimilatory metal-reducing bacteria and antagonistic methanogens is critical for efficient hydrogen production in MEC reactors. Copyright © 2014, Hydrogen Energy Publications, LLC. Published by Elsevier Ltd. All rights reserved.

# 1. Introduction

It is now largely accepted that the dependence on fossil fuels as our primary energy carrier is contributing to global climate changes, environmental degradation and health problems [1,2]. Renewables are thus gaining more importance as an alternative pollution-free solution for the future, worldwide [3]. The United States, for instance, among the largest energy

<sup>\*</sup> Corresponding author. State Key Laboratory of Urban Water Resource and Environment, Harbin Institute of Technology (SKLUWRE, HIT), Harbin, China.

<sup>\*\*</sup> Corresponding author. Tel.: +86 13796629968.

E-mail addresses: liuwz0326@126.com (W. Liu), waj0578@hit.edu.cn (A. Wang).

<sup>&</sup>lt;sup>1</sup> Authors contributed equally to this manuscript.

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and fossil fuel consumers, are starting to face several energyrelated challenges, such as economic and energy growth, energy security, and climate protection [4]. Because of potential risks to the U.S.'s reliance on fossil fuels (i.e., inability to produce sufficient fuel) there is an urgent need for new sources of renewable energy too. Clearly those are issues of global concern, thus besides the U.S., also the EU, Brazil and China have all launched ambitious programs promoting biofuels in the world [5,6].

Hydrogen (H<sub>2</sub>) is one of the most promising emerging energy carriers, because it is clean, efficient, renewable, and has no  $CO_2$  release or toxic bioproducts [7,8]. Thanks to these qualities, H<sub>2</sub> could replace fossil fuels as the next generation energy carrier [9–11].

Several biological processes can produce biohydrogen [10,12], including photosynthesis, dark fermentation [13], and photo fermentation [14]. Biohydrogen production via dark fermentation is one of the most efficient methods (with a stoichiometric potential of 12 mol H<sub>2</sub>/mol [15]) and has been intensely studied [10], although the practical yield is relatively low (usually between 2 and 3 mol H<sub>2</sub>/mol<sub>glucose</sub>) and results in production of several so-called "dead end" products (i.e., acetate and other fermentation products such as butyrate and alcohols) [15], which cannot be further oxidized through dark fermentation without additional energy input, due to thermodynamic limitations [16,17].

A new alternative process for biohydrogen production is electrohydrogenesis, which uses exoelectrogenic bacteria in microbial electrolysis cells (MECs) able to utilize the dead end products, derived from fermentation, to produce additional hydrogen [7,17] and further oxidize the substrate obtained from the dark fermentation effluent.

Generally, the MEC consists of an anode which accepts electrons from the microbial culture, and a cathode, which transfers electrons to an electron acceptor (proton) under anaerobic conditions [16]. Electrons flow from the anode to the cathode through an external electrical connection. Anode and cathode are typically separated by a semi-permeable membrane, which allows protons released from organic matter to move from the anode to the cathode chamber. At the cathode, electrons and protons combine to form pure H<sub>2</sub>, in the presence of a small amount of external voltage [7]. Recently, a single chamber MEC without a membrane has been developed to produce H<sub>2</sub>, thus potentially reducing the costs of bioreactor setup and simplifying the bioreactor design. Various experimental results demonstrate that single chamber MECs work well for H<sub>2</sub> production [17–19]. However, while MECs appear to be a promising mechanism for efficient biohydrogen production, these systems still suffer from high variability, and little is known regarding the function of microbial populations involved.

To date, most studies of MECs and microbial fuel cells (MFCs) have investigated the microbial composition, using methods such as 16S rDNA sequencing [20–22] and denaturing gradient gel electrophoresis [23,24]. However, while these methods can provide insight about which bacteria are present, it does not provide information on the microbe's functional abilities.

A recent study examined microbial communities in MFCs and MECs, operated under different conditions, using a comprehensive functional gene array [18]. This study indicated that the functional diversity in all reactors was high, even with acetate as the only carbon source, and that the highest hydrogen yield was associated with the highest abundance of genes involved in complex carbon degradation. GeoChip can thus be used to identify a large variety of geochemically important functional genes (such as carbon-, nitrogen- and sulfur-cycling genes, those related to phosphorous utilization, metal resistance, etc.), which can be used for profiling changes in microbial community functional structures under different conditions [18].

In the present study, we used a comprehensive functional gene array, GeoChip 3.0 [25], to examine functional microbial community differences in single chamber MECs producing different amounts of  $H_2$ . The objectives of this study were 1) to develop a suitable microbial community that efficiently produced  $H_2$  using wastewater as inoculum, and 2) to better understand how differences in microbial communities can affect  $H_2$  production.

# 2. Materials and methods

#### 2.1. Reactor setup and operation

All experiments used polycarbonate single chamber reactors with anodes and cathodes as previously described [16,18]. Each reactor was made of a chamber (28.5 mL) and a gas collection tube (14.5 mL), which was placed at the top of the reactor, and was run in MEC mode with the cathode placed against the sealed wall of the reactor, opposite the anode brush, and applying a fixed voltage of 0.7 V.

Fifteen single chamber reactors were set up and inoculated, using domestic wastewater (primary clarifier effluent) from the Norman Wastewater Treatment Plant (Norman, Oklahoma). The minimal medium contained 50 mM phosphate buffer (pH 7.0; conductivity 7.5 mS cm<sup>-1</sup>), 310 mg L<sup>-1</sup> NH<sub>4</sub>Cl, 130 mg L<sup>-1</sup> KCl, a trace nutrient solution (Wolfe's vitamin and mineral solutions), and 1.0 g L<sup>-1</sup> glucose as the sole carbon source.

At startup, reactors were fed a mixture of equal parts wastewater and buffer solution for two (24-h) batch cycles, and then switched to the glucose medium and operated as MECs for one month. The medium was replaced when the current decreased below 0.2 mA, and the reactors were purged with N<sub>2</sub> (99.998%) for 20 min. Reactors were maintained at room temperature (25 °C).

Gases were collected in gas bags (0.1 L capacity; Cali-5-Bond, Calibrated Instruments) for analysis. Gas samples were collected using a syringe (1 mL, Sample-Lock Syringe) from the reactor headspace and the gasbag. Gas chromatography (Agilent 6890N, with N<sub>2</sub> as a carrier gas) was then used to analyze the gases (H<sub>2</sub>, CO<sub>2</sub>, CH<sub>4</sub>). Voltages across a resistor (1.3 ohms) were measured using a multimeter (model 2700; Keithley Instruments). Glucose content was determined at the start and end of each cycle, using high performance liquid chromatography (HPLC, Agilent 1200).

MECs were operated for 56 days to allow microbial communities and functions to stabilize. Based on reactor functioning, five reactors were selected for further study. Every 2-3 days, 26 mL solution was collected from each reactor, centrifuged (8000 rpm), and the resultant pellets were stored at -80 °C for consequent DNA extraction. Since reactor function had stabilized, samples from days 45, 48, and 52 were used as biological replicates.

# 2.2. DNA extraction, amplification, labeling and hybridization

DNA was isolated from cell pellets using a freeze-grinding method [26]. DNA (100 ng) from each sample was amplified using the TempliPhi kit (GE Healthcare) following a modified method [27]. Amplified DNA ( $\sim 2 \mu$ g) was labeled with Cy-5 using random priming with Klenow as described previously [28]. Samples were hybridized to GeoChip 3.0 for 12 h at 42 °C and 40% formamide with mixing on a MAUI Hybridization station (BioMicro, Salt Lake City, UT).

#### 2.3. Data analysis

Hybridized GeoChips were scanned (ScanArray Express Microarray Scanner, Perkin Elmer) and digitally analyzed using ImaGene (6.0 premium version, BioDiscovery, El Segundo, CA, USA). Spots with signal-to-noise ratios (SNR) <2, outliers (standard deviation >3), and poor spots were removed. Data normalization was performed as described previously [28,29].

Cluster analysis was performed using the pairwise average-linkage hierarchical clustering algorithm in CLUSTER (http://rana.stanford.edu) and visualized with TREEVIEW (http://rana.stanford.edu/). The majority of analyses were performed using R with functions in vegan packages [30], with some additional code utilizing vegan installed in our GeoChip analysis pipeline (ieg.ou.edu).

# 3. Results

#### 3.1. Reactor performance

Five sets of reactors (designated as reactors A–E), having differing levels of efficiency (Table 1), were examined. Reactor A was characterized by the highest amount of  $CH_4$  but low  $H_2$ and  $CO_2$  production. Reactor B showed a high production of  $H_2$ ,  $CO_2$  as well as  $CH_4$ . Reactor C obtained the best results, producing the highest amount of  $H_2$  and having the highest CE and CP. Reactor D, instead, had the poorest performance, with little  $H_2$  production and the lowest CE of all reactors. Finally, reactor E had a moderate level of performance. Overall, with the only exception of reactor D, all reactor replicates showed

# Table 2 – Average values of richness, diversity and evenness indexes for each reactor based on GeoChip results.

|               | Shannon                           | Simpson                             | Pielou                            | SimpsonE                          |  |  |  |
|---------------|-----------------------------------|-------------------------------------|-----------------------------------|-----------------------------------|--|--|--|
| Α             | $\textbf{6.66} \pm \textbf{0.51}$ | $\textbf{591.4} \pm \textbf{251.3}$ | 0.96 ± 0.01                       | $0.51\pm0.02$                     |  |  |  |
| В             | $5.07 \pm 0.27$                   | $107 \pm 38.4$                      | $\textbf{0.92} \pm \textbf{0.02}$ | $\textbf{0.43}\pm\textbf{0.06}$   |  |  |  |
| С             | $5.08\pm0.08$                     | $101.5\pm17.5$                      | $\textbf{0.92} \pm \textbf{0.01}$ | $\textbf{0.41}\pm\textbf{0.06}$   |  |  |  |
| D             | $\textbf{5.74} \pm \textbf{0.16}$ | $\textbf{208.8} \pm \textbf{44.9}$  | $\textbf{0.94} \pm \textbf{0.01}$ | $\textbf{0.47} \pm \textbf{0.05}$ |  |  |  |
| Е             | $\textbf{6.58} \pm \textbf{0.17}$ | $494.9\pm67.04$                     | $\textbf{0.95} \pm \textbf{0.01}$ | $\textbf{0.50} \pm \textbf{0.02}$ |  |  |  |
| E = Evenness. |                                   |                                     |                                   |                                   |  |  |  |

fairly stable performances (Fig. S1), with similar levels of gas production and CE (Table 1). Reactors B, C and E grouped together, with the latter showing a higher variability in terms of  $H_2$  production. Reactor A clearly showed the smallest variability.

## 3.2. Community functional diversity

Community functional gene diversity, richness, and evenness of each reactor community were assessed, based on GeoChip results (Table 2). Approximately 2000 different functional genes were detected across all reactors, containing from 250 to 1200 genes each. Highest gene numbers (1000–1200) were detected in Reactors A and E, while the lowest gene numbers ( $\sim$ 250) were detected in B and C. Highest diversity was also noted for A and E, with B and C having the lowest.

#### 3.3. Community structure differences

To visualize differences in overall functional structure, all genes detected by GeoChip were used for cluster analysis (Fig. 1). All clusters contained a variety of functional genes and in general covered most categories contained on the GeoChip. Cluster 3 genes, for instance, were involved in a variety of different functions, such as antibiotic resistance, denitrification, N fixation, organic contaminant degradation, and sulfate reduction.

Results showed that reactors B and C grouped together, thus forming a separate cluster from reactors A, D and E. Based on gene clustering, twelve different groups were detected. Genes from clusters 3, 5, and 8 were detected in all wells. Whereas clusters 1, 2, 6, 7, 9, and 11 were detected in 2 or 3 of the reactors. Finally, some of the clusters were only detected in one reactor, and more specifically: cluster 4 in reactor E, cluster 10 in reactor A and cluster 12 in reactor C.

| Table 1 – Gas production and coulombic efficiency in MEC reactors. |                                   |  |                                   |                                   |                          |  |  |  |
|--|-----------------------------------|--|-----------------------------------|-----------------------------------|--------------------------|--|--|--|
|  | H <sub>2</sub> (mL)               | H <sub>2</sub> yield (mol H <sub>2</sub> /mol <sub>glucose</sub> ) | CH <sub>4</sub> (mL)              | CO <sub>2</sub> (mL)              | Coulombic efficiency (%) |  |  |  |
| А  | $1.89\pm0.86$                     | 0.78 + 0.36  | $5.61\pm0.40$                     | $\textbf{2.19} \pm \textbf{0.24}$ | $59\pm4$                 |  |  |  |
| В  | $\textbf{4.27} \pm \textbf{1.14}$ | 1.67 + 0.47  | $\textbf{5.28} \pm \textbf{0.11}$ | $\textbf{3.36} \pm \textbf{0.16}$ | $61\pm5$                 |  |  |  |
| С  | $12.16\pm1.05$                    | 5.01 + 0.43  | $\textbf{4.83} \pm \textbf{0.26}$ | $\textbf{3.13} \pm \textbf{0.22}$ | $65\pm5$                 |  |  |  |
| D  | $\textbf{0.10}\pm\textbf{0.09}$   | 0.04 + 0.03  | $\textbf{3.71} \pm \textbf{0.41}$ | $1.94\pm0.26$                     | $45\pm1$                 |  |  |  |
| Е  | $5.65\pm2.57$                     | 2.33 + 1.06  | $\textbf{4.57} \pm \textbf{0.26}$ | $\textbf{2.58} \pm \textbf{0.21}$ | $61\pm5$                 |  |  |  |



Fig. 1 — Hierarchical cluster analysis of all genes detected in all reactors. Signal intensities were averaged for replicate reactors. Results were generated in CLUSTER and visualized in TREEVIEW. Red indicates signal intensities above background and black indicates signals below background. Higher intensity reds indicate higher signal intensities. Graphs to the right indicate average signal intensities of each cluster. (For interpretation of the references to color in this figure legend, the reader is referred to the web version of this article.)

DCA was then used to further examine changes in the functional microbial community structure (Fig. 2). In DCA ordination plots, samples that are more similar are closer together, while those that are more different are further apart. The relatively small error bars indicate that replicate reactors had similar community structures. All the reactors separated well, with minimal overlap. As can be seen, reactor A was located furthest from the other reactors, thus indicating that it was the most dissimilar one. The other reactors were more similar but still distinct from each other. Reactors B and C were separated by axis 2, and were clearly distinct from reactors D, E and A (which distributed along axis 1). Dissimilarity testing with Adonis indicated that the

communities from each reactor were significantly different from each other (p = 0.001).

# 3.4. Relative abundance of functional genes

To further examine differences in the microbial communities, the relative abundance of all functional gene groups was also considered (Fig. 3). While genes from all categories were detected in each reactor, there were differences in the relative abundance of gene groups between reactors. In accordance with the cluster analysis, reactors B and C had similar profiles, although gas production in these two reactors was quite different. Same situation was observed for reactors A and E.



Fig. 2 – DCA of all genes detected by GeoChip. Letters indicate reactor name. Error bars are standard deviation of triplicate reactors.

On the other hand, reactors B and E had similar gas productions but relatively different profiles.

Overall, the most abundant functional genes were related to metal resistance, followed by organic remediation, antibiotic resistance and carbon degradation.

## 3.5. Changes in individual functional gene groups

To further investigate the differences in functional structure between reactors, individual gene groups were examined, based on clustering analysis.

#### 3.5.1. Carbon cycling

While all reactors were fed with glucose as the sole carbon source, several genes involved in complex carbon degradation were detected, including genes for degradation of cellulose, hemicellulose, lignin, starch, pectin, and chitin (Fig. S2). Genes for acetogenesis, degradation of cellulose, chitin, hemocellulose, lignin, starch, vanillin, and malate synthase were detected in all reactors. Carbon fixation genes were also detected, including genes for rubisco, carbon monoxide dehydrogenase, and propionyl-CoA carboxylase from a variety of different microorganisms (Fig. S3). A rubisco derived from an uncultured bacterium (gi157679123) was detected in all reactors. Propionyl-CoA carboxylase genes derived from *Roseiflexus* sp. (148657926), *Nitrobacter hamburgensis* (92117653), *Chloroflexus aggregans* (118045694), carbon monoxide dehydrogenase (CODH) from an uncultured bacterium (lab clone), and rubisco derived from an uncultured bacterium (224579026) were also detected in most of the reactors.

#### 3.5.2. Methane

Nineteen genes involved in methane oxidation or methanogenesis were detected across all reactors (Fig. S4). Of these, four were for methane production (*mcrA*) and the remainder for methane oxidation (*pmoA* or *mmoX*). Most of the detected genes were from uncultured bacteria. *mcrA* was detected in most reactors, with the highest number being detected in reactor A, which showed the highest level of methane production, although this reactor also contained the highest number of methane oxidation genes.

#### 3.5.3. N cycling

Genes involved in denitrification, N reduction, N fixation, ammonification, and nitrification were detected in all reactors (Fig. S5–S8). Most of the genes were detected in reactors A and E. The largest part of the denitrification and N fixation genes (nirK, nirS, norB, narG, nosZ) belonged to uncultured bacteria (Fig. S5). Sequences for narG (gi26278770, gi124488241) and nirS (57335474) were detected in all reactors. Sequences for N reduction (nirA, nirB, nasA, nrfA, napA) were mostly detected in reactor A. A nrfA, derived from Desulfitobacterium hafniense



Fig. 3 – Relative abundance of all gene categories covered by the GeoChip. Abundance was calculated by dividing the total signal intensity of each gene category by the total signal intensity of all genes detected.

DCB-2 (gi109645564), and a *ureA*, derived from Ralstonia pickettii 12D (gi151575999), were detected in all reactors. Ammonification and nitrification genes (*ureC*, *amoA*, *hzo*, *gdh*, *hao*) were also detected in most reactors.

#### 3.5.4. Metal resistance

A previous study of *Geobacter sulfurreducens*-MEC indicated an increase in transcription of several metal resistance genes, including efflux transporters for Cd, Co and Zn resistance [31]. In the present study, metal resistance was the most abundant functional gene group (see Fig. 3). Therefore, we decided to examine metal resistance genes more in detail. Genes for resistance to As (arsB, arsC), Cd (cadA, cadBD), Cd, Co, and Zn (czcA, czcD), Cr (chrA), Co (corC), Co and Ni (cnrA, cnrC), Cu (copA, cueO, cusF), Pb (pbrA, pbrD), Hg (merA, merB, merP, merT, metC), Ni (nreB), Ag (silA, silC, silP), Te (tehB, terC, terD, terZ), and Zn (zitB, zntA) were detected and most of these genes were found in all reactors, as can be seen in Fig. S9.

#### 3.5.5. Hydrogenases

Hydrogenases catalyze the oxidation/reduction of  $H_2/H^+$ . As these enzymes are involved in the generation of  $H_2$ , we examined them more in detail. Twenty-nine hydrogenase genes were detected across all reactors, with 10 being detected in at least two replicate reactors (Fig. 4). It is worth noting that reactor C, which had the highest  $H_2$  production rates, contained the fewest hydrogenases. Hydrogenases derived from Dehalococcoides ethenogenes 195 (57233678), Desulfovibrio desulfuricans subsp. desulfuricans (220904110), Desulfovibrio fructosovorans (186883006). Shewanella baltica OS223 (217498707), and Rhodobacter sphaeroides (126462908) were detected in all reactors. Hydrogenase genes are designed principally related to hydrogen generation (proton reduction) in GeoChip. However, their detection in the anode communities was assumed to contribute to proton reduction in fermentation process. But the fact was that the least hydrogenase genes were detected in reactor C with the highest hydrogen yield, indicating that hydrogen conversion would not be determined primarily by fermentation metabolism. Therefore, hydrogen production was significantly controlled by electron transporting process in MECs.

#### 3.5.6. Cytochromes

In total, 105 cytochrome genes were detected in all reactors, with 32 being detected in at least two replicate reactors (Fig. 5). According to the hierarchical cluster analysis of cytochrome genes, reactor C resulted to be distinct from the other reactors. Only one cytochrome sequence, derived from *Geobacter metallireducens* GS-15 (78221556, involved in Fe(III) respiration), was detected in all reactors. Cytochromes derived from *Bradyrhizobium* sp. (146190249, involved in oxidation of organic contaminants) and *G. sulfurreducens* (39995384, *OmcA/MtrC*) were also detected in most reactors.

Several cytochrome c genes are known to be involved in electron transport mechanism in microbial fuel cells, including the outer membrane associated metal reductases, *OmcB* (MtrC) and *OmcA* [32]. In the present study *OmcA*/MtrC from *G*. *sulfurreducens* (39995699, 39997094, 39996436), *Shewanella sediminis* 



Fig. 4 — Hierarchical cluster analysis of hydrogenase genes. Signal intensities were averaged for replicate reactors. Results were generated in CLUSTER and visualized in TREEVIEW. Red indicates signal intensities above background and black indicates signals below background. Higher intensity reds indicate higher signal intensities. (For interpretation of the references to color in this figure legend, the reader is referred to the web version of this article.)





Fig. 6 – Abundance of cytochrome genes detected in the 5 reactors by GeoChip. Green line indicates the relative abundance of total cytochrome genes (as % of all genes), while the yellow line shows the relative abundance of cytochromes known to be involved in electron transport in MECs (as % of all cytochrome genes). Bars indicate the total signal intensity of total cytochromes (in purple) and of those involved in electron transport (in blue), respectively. (For interpretation of the references to color in this figure legend, the reader is referred to the web version of this article.)

(157374666, 157374665), Shewanella oneidensis (24373227), Shewanella amazonensis (119774348), Shewanella loihica (127513452), and Shewanella pealeana (157960153, 157962516) were detected in the reactors. Flavocytochromes (which act as electron shuttles) from S. baltica (126172505, 126172508) and S. loihica (127511210) were also detected. Other cytochrome genes included DmsE (DMSO reduction), NapB, NapC (both for nitrate reduction), P450 (oxidation of organic contaminants), LivK (manganese oxidation), CoxB (oxidative phosphorylation) and others involved in metal reduction, aerobic respiration, sulfite oxidation, and cytochrome assembly.

A similar relative abundance of cytochrome genes (% of total gene abundance) was detected across all reactors (ranging from 1.3 to 1.8%; Fig. 6). Reactor C, which had the highest  $H_2$  production, showed a higher (total) amount of cytochrome genes, although the abundance of cytochrome genes involved in electron transport (including outer membrane associated metal reductases and flavocytochromes) were higher in reactors D and E.

Since exoelectrogenic bacteria are often capable of metal reduction, metal reducing strains were also further examined. Cytochrome *c* genes derived from 28 different microbial strains were detected in the reactors (Fig. S10). Among these, Anaeromyxobacter dehalogenans 2CP-C, Bradyrhizobium sp. ORS278, D. desulfuricans G20, G. metallireducens GS-15, G. sulfurreducens PCA, Shewanella denitrificans OS217, Shewanella frigidimarina NCIMB 400, S. sediminis HAW-EB3, and Shewanella sp. were detected in all reactors.



Fig. 7 – CCA of all genes detected by GeoChip and reactor productivity values. Circles indicate reactors, letters and numbers indicate reactor names; arrows indicate productivity measures (Factors:  $H_2$  for hydrogen,  $CO_2$  for carbon dioxide, and  $CH_4$  for methane, CE for coulombic efficiency).

# 3.6. Relationship between gas production and microbial community structure

Canonical Correspondence Analysis (CCA) was used to determine how gas reactor performance variables (gas production and coulombic efficiency) were affected by the community structure. Coulombic efficiency referred to the recovery of electrons, defined as the fraction of electrons recovered as current versus that present in the starting organic matter. Variance inflation factors (VIFs) for all variables examined were less than 4.5, indicating that the variables were independent. The model was significant (p = 0.002) and explained 30.4% of the variation (sum of all Eigenvalues, 1.444) (Fig. 7). The first canonical axis was positively correlated with H<sub>2</sub> and CO<sub>2</sub>, and negatively correlated with CH<sub>4</sub>. The second canonical axis was negatively correlated with CO2, coulombic efficiency and methane, and to a lesser extent also with H<sub>2</sub>. Reactors B and C (but also E) were positively correlated with CO<sub>2</sub> and H<sub>2</sub>, with CO<sub>2</sub> showing the strongest correlation. Reactor A was positively correlated with CH<sub>4</sub>, while reactor C (and to a lesser extent also reactor B) was positively correlated with coulombic efficiency.

Further, Variance Partitioning Analysis (VPA) [33,34] was performed to better understand how much each of the

Fig. 5 — Hierarchical cluster analysis of cytochrome genes. Signal intensities were averaged for replicate reactors. Results were generated in CLUSTER and visualized in TREEVIEW. Red indicates signal intensities above background and black indicates signals below background. Higher intensity reds indicate higher signal intensities. (For interpretation of the references to color in this figure legend, the reader is referred to the web version of this article.)

performance variables were influenced by the community structure. When CH<sub>4</sub>, CO<sub>2</sub>, and coulombic efficiency were held constant, there was only a weak correlation (p = 0.082) between H<sub>2</sub> production and the community structure. When H<sub>2</sub> and coulombic efficiency were held constant, CH<sub>4</sub> and CO<sub>2</sub> showed a significant correlation (p = 0.002). H<sub>2</sub> was able to independently explain 7.6% of the variation observed, CH<sub>4</sub> and CO<sub>2</sub> independently explained 23.8%, and coulombic efficiency, while not significant (p = 0.150), was able to independently explain 7.9%. There was some interaction between H<sub>2</sub>, CH<sub>4</sub> and CO<sub>2</sub> (4.5%), and between CH<sub>4</sub> and CO<sub>2</sub> and coulombic efficiency (1.7%) as well. Over half of the variation (55.9%) remained unexplained.

# 4. Discussion

#### 4.1. H<sub>2</sub> production in MECs

All of the MEC reactors examined in this study were able to produce  $H_2$  at room temperature with 1 g/L glucose as the only added carbon source. Glucose fermentation produces several acids (e.g., acetic and lactic acids), which can, in turn, generate additional  $H_2$  in the MEC.

Even though all reactors were inoculated with the same starting material and were treated in the same way (same parameters, carbon source and medium), the efficiency of  $H_2$  production and total yield varied greatly between reactors (from 0.10 to 12.2 mL  $H_2$ , with a yield ranging from 0.04 to 5.01 mol  $H_2$ /mol<sub>glucose</sub>), thus implying a large variability in the biofilm formation process. This further suggests that anode community development might be a very stochastic process, not directly associated to the controlled parameters, and that an enrichment phase might be useful (especially when using a complex inoculum, such as wastewater).

Clearly there could be several reasons for differences in the H<sub>2</sub> production. Hydrogenases catalyze the reversible oxidation of  $H_2$ ; they can produce  $H_2$  or use it. Several hydrogenases were detected in all reactors, but detection of the genes does not indicate whether the reaction is catalyzing H<sub>2</sub> production or utilization. Moreover, methane production can also consume H<sub>2</sub> [35]. This methane is most likely obtained from hydrogenotrophic methanogenesis, since there was insufficient time to form a methanogenic biofilm [36]. In our reactors, higher methane levels tended to correlate with lower H<sub>2</sub> levels (as confirmed by the Canonical Correspondence Analysis), although this was not always the case, probably because H<sub>2</sub> can also be consumed by chemolithotrophic bacteria [37]. The presence of H<sub>2</sub>-consuming bacteria might also explain why, despite the interesting  $H_2$  yield (about 5 mol  $H_2$ /mol<sub>glucose</sub>), a previous study by Cheng and Logan [19] reported performances of up to 8.55 mol H<sub>2</sub>/mol<sub>glucose</sub> (while methane was detected only in traces), at an applied voltage of 0.6 V.

Despite the differences among the reactors A–E, these results showed that wastewater represents a suitable inoculum for effective  $H_2$  production with MEC technology. However a suitable treatment to inhibit the growth of  $H_2$ -consuming bacteria would clearly further enhance yields. In fact, while the use of single-chamber reactors allows for a simple reactor design, on the other hand we must also consider that the lack of membrane can reduce  $H_2$  recoveries, due to  $H_2$  consumption by microorganisms in the wastewater [35].

#### 4.2. Functional gene diversity

While reactors in this study were fed only glucose, the functional diversity was quite high in all reactors (in accordance with Liu et al. [18], who used acetate as the sole carbon), both in terms of diversity indices and number of different functional gene categories detected. Genes from all major functional categories were detected in all reactors, indicating that the microbial communities were able to perform a large variety of functions. This was expected, due to the use of wastewater as inoculum.

According to the Canonical Correspondence Analysis, used to determine how gas reactor performance variables were affected by the community structure, reactors B, C and E positively correlated to H<sub>2</sub>. Reactors B and C also positively correlated to coulombic efficiency. However, we did not observe a correlation between diversity and H<sub>2</sub> production. In fact, the reactor with the highest H<sub>2</sub> production (reactor C) had the lowest diversity, while another reactor with a similar diversity performed only moderate level of H<sub>2</sub> production. This suggests that variability was not necessarily (only) related to the presence of electrochemically active bacteria, as a fraction of the biofilm can be formed by non-exoelectrogens, such as fermentation and or symbiotic relationships with other bacteria [38]. This also suggests that probably some important "non-exoelectrogenic" functions, involved in H<sub>2</sub> production (such as formate-liase enzymes), were not taken into account.

Clearly, the presence of  $H_2$ -consuming bacteria might also add an important contribution to the diversity of the diversity of the community: in fact, according to the Variance Partitioning Analysis (VPA), variability of methane producers explained up to 24% of the variation, against only 7.6% for  $H_2$ . This might explain why  $H_2$  production was not associated to biodiversity, since a large part of variability was associated to methane producing organisms.

In any case, as already mentioned, differences in reactor performance could also be linked to a different development of the exoelectrogenic bacterial community among the different biofilms, as well as to the different microbe's position within the biofilm itself, thus underlining the importance of biofilm structure, such as stratification of functional groups [38].

#### 4.3. Key microbial populations involved in H<sub>2</sub> production

The overall community structure was fairly different between reactors (Figs. 2, 3 and 7), and there were distinct differences which may help identifying populations important for (or detrimental to) overall  $H_2$  production.

It is well known that specific cytochromes are essential [39,40] for bacteria, such as Shewanella [32] and Geobacter strains [31], to extracellularly transfer electrons to the electrode. Shewanella, for instance, is able to transfer electrons to the anode via the multiheme c-type cytochromes MtrC (OmcB) and OmcA [32]. These cytochromes were detected in all reactors. Other cytochrome genes derived from several known exoelectrogenic genera, including Anaeromyxobacter, Desulfovibrio [41], Geobacter [42], and Shewanella [43] were also

detected. The same genera were previously detected in MEC reactors with acetate as the sole carbon source [18]. Other functional genes from genera known to be exoelectrogens, such as *Clostridium*, *Desulfovibrio*, *Escherichia*, *Geobacter*, *Pseudomonas*, *Rhodopseudomonas*, and *Shewanella* spp. were present in all reactors examined in this study. In addition, flavins, which can act as electron shuttles [32], were also detected. The presence of these functional genes explains the ability of all reactors to produce H<sub>2</sub>.

Clearly, as already mentioned, methane production is still a problem in MEC's with mixed cultures [44], because the metabolism of methanogens can decrease the amount of  $H_2$ detected and/or produced, either through  $H_2$  consumption to produce methane or substrate consumption. As such, methods to reduce the amount of methane produced in reactors are desirable to increase  $H_2$  yields [35]. In fact, reactors with the highest  $H_2$  production had the least amount of methanogens.

Another population of interest consists of hydrogenase containing bacteria, since they can either use or produce H<sub>2</sub>. Compared with the other reactors, Reactor C had considerably higher exoelectrogenic bacteria (such as *Shewanella, Geobacter*), less methanogens and less hydrogen-utilizing bacteria. This is consistent with observations that the highest hydrogen yield was obtained in this reactor, and confirms the importance of dissimilatory metal-reducing bacteria such as *Geobacter* and *Shewanella* species [38].

#### 4.4. MECs and wastewater treatment

In the present study, many carbon degradation and contaminant degradation genes were detected, suggesting that a wide range of carbon sources could be utilized by the microbial community. In addition, several functional capabilities, found in the reactors investigated in this study, would be useful in wastewater treatment. Organic contaminant degradation related genes can remove contaminants by metabolizing them to nontoxic substrates, which can then be utilized by other microorganisms. Toxic metals can be reduced by microorganisms, to remove them from solution, or could be sequestered by excreted substances such as sulfide from sulfate-reducing bacteria. Genes for degradation of herbicides and pesticides, solvents, and chlorinated compounds were detected. Phosphorus utilization, sulfate reduction, and nitrogen reduction genes were also detected, which would be all useful in wastewater treatment [45-47].

For this reason, the selected microbial community might represent a suitable inoculum not only for  $H_2$  production, but also for a concomitant effective wastewater treatment.

In fact, wastewater still contains organic material that can provide suitable nutrition for both, exoelectrogenic and nonexoelectrogenic microbes. The latter could then be helpful to remove contaminants, such as toxic compounds (present in wastewater) that must be treated prior to disposal.

It is worth noting that successful biological  $H_2$  production depends on the overall performance (results of interactions) of the bacterial community in the reactor. Therefore, metabolic cooperation within the bacterial community may provide useful combinations of metabolic pathways for the processing of complex waste material (and the degradation of impurities and/or inhibitors), thereby supporting a more efficient decomposition of substrate [48–51].

Therefore, the great advantage of coupling wastewater treatment with MECs would be that extra hydrogen is recovered, while the wastewater is treated by removing organic matter and contaminants through oxidation [35,45–47].

# 5. Conclusion

In this study we have developed an effective community for hydrogen production, able to produce up to 5.01 mol H<sub>2</sub>/mol<sub>glucose</sub> (reactor C), using wastewater as inoculum. Maximum coulombic efficiency reached 65 ( $\pm$ 5)%. GeoChip-based metagenomic analysis allowed to observe a large variety of microbial functional genes, with approximately 2000 different functional genes detected across all reactors. H<sub>2</sub> production correlated with the community structure, but not with the diversity. The most abundant functional genes detected were related to metal resistance, followed by organic remediation, antibiotic resistance and carbon degradation. Reactor C, with the best performance, had considerably higher exoelectrogenic bacteria (e.g. Shewanella, Geobacter), less methanogens and less hydrogen-utilizing bacteria, compared with the others. These results suggest that wastewater represents a suitable inoculum for effective H<sub>2</sub> production with MEC technology, however a suitable treatment to inhibit the growth of H<sub>2</sub>-consuming bacteria (such as methanogens) would clearly allow to further enhance the yields. Further, these results also showed that GeoChip can provide useful information for the characterization of complex microbial communities and that MEC can be considered a promising technology to produce hydrogen from wastewater.

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#### Appendix A. Supplementary data

Supplementary data related to this article can be found at http://dx.doi.org/10.1016/j.ijhydene.2014.01.001.

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